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Humic acid-induced formation of tobermorite upon hydrothermal treatment with municipal solid waste incineration bottom ash and its application for efficient removal of Cu(II) ions

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2	municipal solid waste incineration bottom ash and its application for efficient removal of		
3	Cu(II) ions		
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Humic acid-induced formation of tobermorite upon hydrothermal treatment with

# **Abstract**

In this study, conversion of municipal solid waste incineration bottom ash (IBA) into highly efficient sorbents for Cu(II) removal was reported. The formation of tobermorite induced by humic acid (HA) and IBA under hydrothermal condition was explored and its potential application for efficient removal of Cu(II) ions was further investigated. After hydrothermal treatment, the morphology and microstructure of IBA remarkably changed from sheet-like to particle-like, thereby resulting in substantial increases of sorption capacity. The synthesized tobermorite exhibited a strongly enhanced sorption performance toward Cu(II), which was 270.3 mg g<sup>-1</sup> and higher than other reported sorbents. The adsorption behaviors were subsequently examined by isotherm and kinetic studies. Langmuir model was found to describe the adsorption process well, suggesting that the adsorption was chemisorption in nature. Therefore, the hydrothermally synthesized tobermorite may be used as sorbents to remove Cu(II). Conversion of IBA into valuable minerals recovers waste into potential resources and alleviates the needs for ash disposal.

- Keywords: Municipal solid waste (MSW); incineration bottom ash (IBA); humic acid;
- 36 hydrothermal treatment; heavy metals

## 1. Introduction

In recent years, the growing generation of municipal solid waste (MSW) has become a great burden to the society because it raises serious environmental and economic concerns (Bai and Sutanto, 2002). Incineration of MSW is an effective approach to reduce the volume and

mass of waste by about 90% and 70%, respectively (Chimenos et al., 1999). It is also an important component of the integral management of MSW to recover energy from waste. Incineration bottom ash (IBA) is the major by-product during the incineration process and accounts for 85-95% of all residues by volume (Luo et al., 2017a). In the USA, most of the IBA is disposed of by landfilling, while in some European and Asian countries about 50% of the IBA is utilized as secondary building materials for road construction and cement production (Hjelmar, 1996). To prolong the lifespan of landfills and to recover waste into resources, it is of great interest to recycle and upgrade IBA.

Hydrothermal method is an attractive means to convert wastes into valuable products (Luo et al., 2018). For example, given an appropriate Ca/Al/Si ratio, new mineral phases such as katoite, zeolite and tobermorite can be formed upon hydrothermal treatment using IBA as a starting material (Penilla et al., 2003; Wang et al., 2016). The sources of IBA, activation solution, and reaction temperature and time strongly affect the formation of those secondary mineral phases (Etoh et al., 2009). The main chemical reactions involved in the hydrothermal transformation of IBA inorganic matters are the dissolution of SiO<sub>2</sub> and Al-containing minerals that followed by re-precipitation with Ca-minerals under highly alkaline conditions (Jing et al., 2013). It is well known that IBA also contains a few percentage of organic matters because sometimes they are not completely oxidized by incineration and the partially unburned organic waste materials will co-exist with subsequent formation of new organic compounds (Dugenest et al., 1999).

The organic matters in IBA substantially govern the hydrothermal conversion of IBA into different new mineral products and therefore play a crucial role in IBA recycling and utilization.

According to the classification of soil organic matter, the organic matters in IBA can be divided into humic substances and non-humic substances. Humic substances are mainly composed of humic acid (HA) and fulvic acid (FA), which have been identified as an important fraction of dissolved organic carbon (DOC) contributing to the complexation of contaminants (Olsson et al., 2007). Besides its presence in IBA, HA has also been found to widely exist in the natural environment and it has a relatively high affinity for binding heavy metals and organic pollutants (Luo et al., 2015). A previous study suggested that HA and FA contributed to 0.3-0.6% and 14-26% of DOC in the leachate from IBA, respectively (Van Zomeren and Comans, 2004). As a typical natural organic matter (NOM), HA can substantially govern the IBA recycling and utilization through binding with heavy metals. Although the role of HA in the hydrothermal conversion of IBA remains unknown, HA would bind heavy metal ions and therefore alter the leaching behavior of IBA.

Mostly, IBA is hydrothermally converted into super-porous layered structures or fine particles and crystals, thereby showing excellent adsorption performance due to high specific surface area and ion-exchange capacity (Jing et al., 2007; Wang et al., 2016). The alkaline condition is more favorable to activate the hydrothermal reactions and HA is supposed to participate. The reaction products are subsequently employed as sorbent materials for efficient removal of metal ions and organic dyes from aqueous solution (Wang et al., 2016). Hence, hydrothermal transformation of IBA into sorbent provides a solution to reduce the needs for ash disposal. So far, the HA-involved hydrothermal process of IBA is not well documented and understood. The effect of HA on hydrothermal reaction of IBA and the underlying mechanisms remain unclear.

The main objective of this study is to explore the formation of tobermorite induced by humic acid (HA) and IBA under hydrothermal condition and to further investigate its potential application for efficient removal of Cu(II) ion, a typical hazardous heavy metal in water. The layer-structured IBA was converted into particle-like mineral phases through hydrothermal reaction, thereby showing superior sorption performance toward heavy metals. The chemical, morphological and mineralogical properties of raw IBA and the converted tobermorite were characterized. The adsorption behaviors were subsequently examined by isotherm and kinetic studies. Langmuir model was used to describe the adsorption process, in which chemisorption was determined. Together, these experimental results are of environmental significance because they recover waste into potential resources and alleviate the needs for ash disposal.

#### 2. Materials and methods

#### 2.1. Production, collection and sorting of IBA

MSW-derived IBA samples were obtained from a local Waste-to-Energy (WTE) incineration plant in Singapore, which can treat 800 tons of MSW and generate 2.2×10<sup>7</sup> Watts of green energy every day. According to the data from National Environment Agency (NEA), Singapore, about 7.70 million tons of MSW was generated and 4.72 million tons of MSW was recycled in the year of 2017. The other 2.98 million tons of MSW was disposed and burned consistently without pre-processing at a temperature of 800-1000°C. Waste sources are mainly domestic, including plastics (~25.62%), food waste (~22.71%), paper/cardboard (~19.33%), ash/sludge (~7.21%), textile/leather (~4.74%), horticultural waste (~3.61%), wood (~3.27%),

glass (~1.98%), construction debris (~0.32%), ferrous metal (~0.26%), used slag (~0.10%), scrap tyres (~0.10%), non-ferrous metals (~0.05%), and others (stones, ceramic, rubber, etc., ~10.70%). During incineration, the air-cooled multi-stage grate was the only grate combustion system and the water-cooled multi-stage grate was designed for combustion of higher calorific wastes. To prevent the formation of dust, water was splashed on IBA after the incineration.

IBA can be highly heterogeneous and the properties of IBA may vary with time. To obtain representative IBA samples, 20 kg of fresh IBA was collected once every two weeks from the WTE facility and over a period of five months. After each collection, the fresh IBA was immediately dried in an oven at 105°C for 24 h to remove surface moisture and then sealed to minimize carbonation (Luo et al., 2017a). Altogether, approximate 200 kg of dry IBA was sampled over five months and mixed by a planetary mixer. Prior to use, the 5-month combined IBA was sieved into four size fractions, i.e., < 0.30 mm; 0.30-1.18 mm; 1.18-6.30 mm; and > 6.30 mm. Each size fraction accounts for about 25% of the total weight of IBA. In the current study, < 0.30 mm size fraction was used for subsequent experiments because smaller particles possess higher specific surface area and are more effective for preparation of sorbent materials.

## 2.2. Hydrothermal synthesis of IBA-based materials

The hydrothermally treated IBA was prepared according to a previous procedure established by the authors (Luo et al., 2017a). The hydrothermally treated (IBA+HA) was synthesized using IBA and humic acid (HA) as the starting materials, no additional Ca, Si and Al elements were introduced. HA was purchased from Sigma-Aldrich Company and was used without further purification. Experiments were performed in a 50 mL Teflon-lined acid

digestion bomb (Parr Instrument Company, USA). The procedures are described as follows: 7.0 g IBA particles were mixed with 35.0 mL reaction solutions, which contained 2.5 M NaOH and different concentrations of HA (10 and 100 ppm, respectively). The mixtures were allowed to stir and react for 30 min at 25°C. The slurry was then transferred into a stainless steel autoclave, carefully sealed and incubated under 180°C for 24 h in the oven. After the hydrothermal reactions, the products were cooled to room temperature and washed three times by repeated centrifugation (5 min at 9000 g, 25°C) using deionized water. The supernatant was discarded and the precipitate was dried in oven at 105°C for 8 h to recover the porous composite material. The mixture of (IBA+HA), which was obtained by mixing 7.0 g IBA with 35.0 mL of 100 ppm HA at pH 7.2 without hydrothermal treatment, was also prepared. The mixture was allowed to react and equilibrate at 25°C on an orbital shaker (SKF-3100, Jeio Tech) under 200 rpm for 24 h. The reaction product was similarly collected as described above. The non-treated IBA (< 0.30 mm) were characterized and tested as control samples.

# 2.3. Characterizations of the HA and IBA samples before and after hydrothermal treatment

The chemical compositions of the raw IBA were determined using the sequential X-ray fluorescence (XRF) spectrometer (S8 Tiger, Bruker). IBA (< 0.3 mm) samples in loose powder form were analyzed as pressed pellets with the pre-calibrated standard method. Table 1 summarizes the XRF results. As can be seen, IBA used in the current study mainly consists of CaO (54.06%), SiO<sub>2</sub> (8.24%), and Al<sub>2</sub>O<sub>3</sub> (6.85%). High amount of CaO in IBA (< 0.3 mm) is due to the presence of Ca-containing solid wastes such as food waste, which easily broke down into smaller particles during incineration. SiO<sub>2</sub> and Al<sub>2</sub>O<sub>3</sub> in IBA originate from Si- and Al-

containing solid wastes, e.g., glassware and baverage cans, respectivley. Ferrous metals are recovered after incineration through magnetic separation in the incineration plant and thus content of ferrous oxide in IBA is limited.

The morphological characteristics of the IBA-based materials were observed by imaging with a field emission scanning electron microscope (FESEM, JSM-7600F, JEOL). The experimental samples were pre-treated by gold coating before the test.

The UV-vis spectra of the HA and IBA samples before and after hydrothermal treatment were recorded in the range of 200-800 nm using UV-vis spectrophotometer (UV-2600, Shimadzu). The infrared (IR) spectra of the HA and IBA samples before and after hydrothermal treatment were further characterized in the range of 400-4000 cm<sup>-1</sup> on a Nicolet iS50 FT-IR spectrometer (Thermo Scientific, USA).

Powder X-ray diffraction (XRD) patterns were collected on a Bruker AXS D8 advance diffractometer using Cu K $\alpha$  radiation ( $\lambda$  = 0.154 nm) with the tube voltage of 40 kV and the current of 40 mA. The XRD diffraction patterns were acquired in the 2 $\theta$  range of 5-80° at a scan speed of 2° min<sup>-1</sup>. The phase identification was performed by searching the International Center for Diffraction Data (ICDD) and matching with those included in the Joint Committee on Powder Diffraction Standards (JCPDS) files.

Upon the Brunauer-Emmett-Teller (BET) nitrogen adsorption-desorption isotherms, the specific surface area was determined through an automated surface area and pore size analyzer (Quadrasorb evo, Quantachrome Instruments). The pore size distribution was calculated according to the desorption Barrett-Joyner-Halenda (BJH) method. The outgas temperature

was set at 180°C and the outgas time was 18 h. Data analysis was carried out using the QuadraWin software.

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# 2.4. Batch sorption experiments toward Cu(II)

The batch sorption experiments were performed to investigate the sorption kinetics and isotherms of the IBA materials toward Cu(II) in aqueous solution. Cu(II) ion was used in the form of Cu(NO<sub>3</sub>)<sub>2</sub>. The sorption kinetics were obtained by adding 0.1 g of the IBA samples into 50 mL working solutions with two different initial Cu(II) dosages of 100 and 500 mg g<sup>-1</sup>. These two concentrations were tested in order to estimate the maximum absorption capacity and the incubation time required to reach the adsorption equilibrium. All assays were prepared in triplicate and error bars were calculated according to the standard deviation of triplicate samples. Control experiments were similarly performed without IBA sorbents. The solution pH was adjusted to 5.0 using 2 wt.% HNO3 or NaOH. The reaction solutions were stirred and incubated at 25°C over a period of 10 h on the orbital shaker under 250 rpm. At specified time intervals, 1 mL of the reactant was taken and sacrificed to quantify the residual and sorbed concentrations of Cu(II). Prior to analysis, samples were immediately diluted ten times and filtered through 0.2-µm Acrodisc polyethersulfone membrane syringe filters (Pall Corp., Singapore). The concentrations of Cu(II) ion in the solutions were determined using an inductively coupled plasma-mass spectrometer (ICP-MS, ELAN DRC-e, PerkinElmer). To further obtain the sorption isotherms of Cu(II) onto the IBA materials, batch sorption

experiments were conducted using 100 mL shaking flasks, in which 50 mL of Cu(II) working

solutions and 0.1 g of different IBA samples were added. The initial Cu(II) concentrations in

the solutions were designed from 50 to 1000 mg L<sup>-1</sup>. The reactants were mixed together, and subsequently allowed to react and equilibrate at 25°C for 24 h on the orbital shaker under 250 rpm. To prevent the precipitation, the solution pH was adjusted to 5.0. After equilibration, the concentrations of remaining free Cu(II) ions in the solutions were measured and the adsorption amounts of Cu(II) by the IBA materials were calculated.

The adsorption processes of Cu(II) from aqueous solution onto the IBA materials were described by the Langmuir isotherm equation (Luo et al., 2016). Following are the original form (Eq. 1) and a linearized form (Eq. 2) of the Langmuir isotherm:

$$q_e = \frac{bq_{\text{max}}C_e}{1 + bC_e} \tag{1}$$

$$\frac{C_e}{q_e} = \frac{C_e}{q_{\text{max}}} + \frac{1}{bq_{\text{max}}} \tag{2}$$

where  $C_e$  is the residual Cu(II) concentration at equilibrium (mg L<sup>-1</sup>);  $q_e$  is the amount of Cu(II) adsorbed at equilibrium (mg g<sup>-1</sup>);  $q_{max}$  is the maximum adsorption capacity of the IBA materials at equilibrium (mg g<sup>-1</sup>); and b (L mg<sup>-1</sup>) is the Langmuir constant (Luo et al., 2014; Wang et al., 2016).  $C_e/q_e$  and  $C_e$  were measured experimentally and  $q_{max}$  can be derived by plotting  $C_e/q_e$  in the y-axis against  $C_e$  in the x-axis. Linear fitting between  $C_e/q_e$  and  $C_e$  was then carried out to determine the slope of the line.  $q_{max}$  was calculated by taking the inverse of the slope of the line.

## 3. Results and discussion

## 3.1. Morphology of IBA and its composite materials with HA

Fig. 1 shows the morphology of the raw and hydrothermally treated IBAs at different magnifications. The sheet-like microstructures of the raw IBA were relatively solid and dense in Fig. 1a (top row), whereas those of the hydrothermally treated IBA in Fig. 1b (bottom row) were much more porous with aggregation of fine crystals and particles on the surface. As can be seen, the morphology of IBA remarkably changed after the hydrothermal treatment, which was consistent with previous studies (Jing et al., 2010). The morphological changes of IBA could be attributed to the formation of new crystal phases through dissolution of SiO<sub>2</sub> and Alcontaining minerals and subsequent re-precipitation with Ca-minerals under highly alkaline conditions (Luo et al., 2017a). As a result, the reaction products might contain zeolite, katoite and gehlenite (Pena et al., 2006).

Fig. 2 shows the morphology of the composite materials synthesized by IBA and HA. The IBA-HA complex in Fig. 2a (top row) was obtained without hydrothermal treatment and its morphology exhibited the layered structures with aggregation of solid and dense sheets, which was similar to that of the raw IBA in Fig. 1a. The microstructures of the composite material that combined with IBA and 10 ppm HA after hydrothermal treatment were presented in Fig. 2b (middle row). As can be seen, a mixture of the smooth sheets and fine particles was observed in Fig. 2b, suggesting HA was able to promote the morphological transformation of IBA from sheets to particles. This could be confirmed by further analysis of Fig. 2c (bottom row), in which another composite material that combined with IBA and 100 ppm HA mainly consisted of fine particles after hydrothermal treatment. Thus, the increased dosage of HA resulted in the formation of more fine particles under hydrothermal conditions. The hydrothermally treated IBA without HA addition in Fig. 1b also provided evidence to support this conclusion. A

possible explanation for the effect of HA was that the addition of HA would contribute to the dissolution of IBA in the presence of alkali by complexing with the metal ions and therefore effectively prevent the deposition of altered mineral phases on the surface of original IBA samples.

## 3.2. Spectroscopic characterizations of HA, IBA and their composite materials

Fig. 3 shows the UV-vis spectra of different species including HA, IBA and their composite materials. As can be seen, the spectra of IBA samples exhibited a continuous decrease with a broad peak for the raw IBA around 252 nm and a sharp crest for the hydrothermally treated IBA at 262 nm. The absorbance of the treated IBA in Fig. 3 decreased much faster than that of the raw IBA, especially at wavelength longer than 262 nm. The UV-vis spectrum of HA was broad, featureless and monotonously decreased with an increasing wavelength (Luo et al., 2017b). The observed differences in the patterns of UV-vis absorption might be attributed to the formation of different mineral crystal structures after hydrothermal treatment and the presence of various organic matters in IBA materials (Luo et al., 2017a).

Fig. 4 shows the FT-IR spectra of HA, IBA and their composite materials. As can be seen, similar patterns were found at larger wavenumbers and the differences in absorption bands were mainly observed between 500-1500 cm<sup>-1</sup> for IBA samples, which could be attributed to the asymmetric and symmetric stretching vibrations of Si-O, Al-O or Si-O-Al bonds (Bai et al., 2008; Penilla et al., 2003). According to previous studies, the intense peaks at 1407, 871 and 712 cm<sup>-1</sup> were associated with the presence of CaCO<sub>3</sub> (Legodi et al., 2001), while the O-H stretching vibration in Ca(OH)<sub>2</sub> occurred at 3633 cm<sup>-1</sup> (Reig et al., 2002). After hydrothermal

treatment with and without HA, all those peaks either disappeared or markedly diminished. At the same time, a new band was present at 957 cm<sup>-1</sup> typically for treated IBA, indicating the hydrothermal reactions likely produced new mineral structures containing Ca, Al and Si (Jing et al., 2013).

As for HA, the broad band at 3300 cm<sup>-1</sup> was assigned to H-bonded OH group. The two peaks occurring at 2919 and 2849 cm<sup>-1</sup> were attributed to the asymmetric and symmetric aliphatic C-H stretching of CH<sub>2</sub> group. The weak peak at 1729 cm<sup>-1</sup> was caused by C=O stretching of COOH group, while another weak band at 1631 cm<sup>-1</sup> was attributed to the aromatic C=C skeletal vibrations and C=O stretching of quinones. The intense peak at 1557 cm<sup>-1</sup> belonged to the aromatic C=C stretching. The obvious band at 1367 cm<sup>-1</sup> was assigned to the C-H deformation of CH<sub>2</sub> and CH<sub>3</sub> groups and/or to the antisymmetric stretching of COOgroup (Luo et al., 2015; Wu et al., 2016).

## 3.3. Mineralogical analysis of IBA and its composite materials with HA

Fig. 5 shows the XRD diffractograms of IBA and its composite materials with HA before and after hydrothermal treatment. As can be seen, the crystal phases in raw IBA (< 0.3 mm) were mainly Ca-bearing minerals such as calcite (CaCO<sub>3</sub>, 29.47°) and portlandite (Ca(OH)<sub>2</sub>, 47.56° and 48.56°). The diffraction peak of quartz (SiO<sub>2</sub>, 26.64°) was not typically observed in raw IBA with size less than 0.3 mm. This finding was in accordance with the analysis of Table 1 and could be further explained by the fact that IBA particles less than 0.3 mm have the highest content of Ca and lowest content of Si than other size fractions. The IBA-HA complex showed a similar XRD pattern as the raw IBA since no hydrothermal reaction took place and the major

mineral phases remained unchanged. However, the composite materials, especially after hydrothermal treatment with 100 ppm HA, exhibited many new characteristic peaks at 2θ of 23.16°, 31.68°, 32.88°, 36.04°, 39.56° and 43.28°, indicating hydrothermal reactions of IBA with HA simultaneously changed the morphology and mineralogy of IBA particles. After matched with JCPDS files and compared with related literatures, the newly formed crystal phases were identified as tobermorite (JCPDS card No. 45-1480 and JCPDS card No. 19-1364) (Jing et al., 2007). Moreover, the use of 100 ppm HA resulted in the highest yield of tobermorite during synthesis of the composite materials considering the intensity of diffraction peak. While many factors may affect the formation of tobermorite, the mole ratio of Ca/Si/Al in IBA is the most important factor. Thus, tobermorite can be synthesized via a suitable pathway using IBA as starting material, as long as an appropriate ratio of Ca/Si/Al is given. Coincided with above FT-IR analysis, the original crystal phases became minor ones or even disappeared and meanwhile new crystal phases were evidently formed after treatment, suggesting an excellent efficiency of hydrothermal conversion for raw IBA. Note that, secondary crystal phases such as gehlenite, katoite and zeolite were not typically found in current study, probably due to different molar ratios of Ca/Al/Si in raw IBA that collected from different sources.

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## 3.4. The BET surface property of IBA and its composite materials with HA

The results of BET tests are shown in Fig. 6. As can be seen, an increase in N<sub>2</sub> adsorption capacity of IBA was observed after hydrothermal treatment, regardless of the presence of HA. The calculated BET surface area was 26.9 m<sup>2</sup> g<sup>-1</sup> for the treated (IBA+HA) and 23.1 m<sup>2</sup> g<sup>-1</sup> for the IBA-HA complex (Fig. 6a), and was 20.5 m<sup>2</sup> g<sup>-1</sup> for treated IBA and 17.9 m<sup>2</sup> g<sup>-1</sup> for raw

IBA (Fig. 6b). The high surface area suggests the evolution of porosity and potential for pollutants removal. As per the instructions from IUPAC, the  $N_2$  sorption isotherms were classified as type IV with a hysteresis loop of type H3 (Thommes et al., 2015). The presence of the hysteresis loop at high relative pressure indicated the mesoporous structure in IBA, whereas the sorption capacity of  $N_2$  was attributed to the micropores at low relative pressure (Figs. 6a and b). The pore volume is indicative of total porosity (cm<sup>3</sup> g<sup>-1</sup>), and further analysis of the cumulative pore volume as a function of pore radius showed that the pore volume of modified IBA increased faster than that of raw IBA, especially at a larger pore radius (Fig. 6c). The differential pore size distribution of IBA was obtained by the Desorption Barrett-Joyner-Halenda (BJH) method (Fig. 6d). The intensity of the sharp peak in Fig. 6d indicates the mesopores with an average radius of  $20.2 \pm 0.1$  Å existed in the IBA materials, and the amount of mesopores increased after hydrothermal treatment. Thus, the hydrothermal treatment may have changed the porosity, the pore structure, and the adsorption capacity of IBA because the reactions can form new mineral materials.

## 3.5. Sorption kinetics and isotherms of Cu(II) from aqueous solution

Fig. S1 shows the sorption kinetics of Cu(II) onto IBA and its composite materials at pH 5.0 under different initial dosages. As can be seen, the adsorption equilibrium was rapidly reached within 2 h of incubation. Meanwhile, over 95% of Cu(II) was removed by the IBA-based materials when 100 mg g<sup>-1</sup> of Cu(II) was added (Fig. S1a). In contrast, the removal ratio decreased to 35%-50% when 500 mg g<sup>-1</sup> of Cu(II) was introduced and the adsorption equilibrium was achieved almost after reaction for 8 h (Fig. S1b). The Cu(II) absorption

capacities within 10 h in Fig. S1b were ranging from approximately 175 to 250 mg g<sup>-1</sup> as treated by different IBA sorbents. It was also found that the composite material, i.e., the HA-induced tobermorite exhibited the fastest removal rate of Cu(II) than other sorbent materials such as raw IBA, the treated IBA and IBA-HA complex. The IBA-HA complex was observed to possess the higher Cu(II) absorption capacity than the treated IBA probably because without hydrothermal conditions, a small fraction of HA could bind or sorb onto the surface of IBA due to its carboxyl and hydroxyl groups, and thus contribute to Cu(II) absorption. Overall, the IBA particles after hydrothermal treatment would be composed of various new mineral phases, possessing higher specific surface area and macro- and mesoporous structures (Chiang et al., 2014; Wang et al., 2016). In this study, the addition of HA further induced the formation of tobermorite and improved its surface properties upon hydrothermal treatment with IBA, thereby resulting in a superior sorption performance toward Cu(II) ions from aqueous solution. Control experiments showed that no sorption occurred on either glassware or filtration systems. Consequently, the observed Cu(II) removal was attributed to the adsorption by IBA materials. The maximum adsorption capacity of IBA materials toward Cu(II) was determined using the Langmuir model. Fig. S2 shows the adsorption data of Cu(II), which can be fitted well into a linearized form of Langmuir isotherm equation (Eq. 2) with the correlation factor of  $R^2 >$ 0.98. This indicated that the adsorption of Cu(II) ions onto the surface sites of sorbents could be modeled by monolayer adsorption and the adsorption process was thermodynamically favorable. Analysis of the data in Fig. S2 further revealed that the maximum adsorption capacity toward Cu(II) was 147.06±8.25 mg g<sup>-1</sup> for the raw IBA (Fig. S2a), 178.57±6.96 mg g<sup>-1</sup> <sup>1</sup> for the treated IBA (Fig. S2b), 212.77±11.36 mg g<sup>-1</sup> for the IBA-HA complex (Fig. S2c), and

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270.27±16.44 mg g<sup>-1</sup> for the treated (IBA+HA) (Fig. S2d). The Langmuir constant (b) was calculated according to the linearized isotherm equation, which was 0.048, 0.028, 0.011, and 0.005 L mg<sup>-1</sup>, respectively. Compared to previous investigations (Chiang et al., 2012; Wang et al., 2016), raw IBA in current study showed a relatively high adsorption capacity because smaller particles were used and higher specific surface area was available. The hydrothermal treatment of IBA, especially with the presence of HA led to a better sorption performance toward Cu(II) due to the HA-induced formation of tobermorite. The comparison of Cu(II) sorption capacity by IBAs and other sorbents is presented in Table 2. As a low-cost waste material, the IBA particles were much more effective in removing Cu(II) than other sorbents such as activated carbon (Demiral and Güngör, 2016), granular sludge (Luo et al., 2014), chitosan (Ngah and Fatinathan, 2008), biochar (Pellera et al., 2012), zeolite (Wang et al., 2008), bentonite (Veli and Alyuz, 2007), goethite (Weng et al., 2008), and cellulose (Shen et al., 2009). These results suggested that IBA, especially after hydrothermal treatment with HA, was a promising sorbent to efficiently remove Cu(II) ions. While the effort to be paid for hydrothermal as proposed in the current study can be high, it may be offset by other factors. For example, in land scarce city, such as Singapore, IBA recycling not only prolongs the lifespan of landfills but also create alternative local resources from wastes. Other tangible and intangible benefits include alleviating the disposal costs of the ash, preserving land capacity, conserving dwindling supplies of natural raw materials, and mitigating potential environmental impacts. In this circumstance, IBA recycling is not only driven by economic sense and government may provide incentives to encourage IBA usage. Further studies, e.g., the leaching

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behavior and the life cycle (cost) assessment, are necessary before practical adoption of the current approach.

## 4. Conclusions

In this study, the formation of tobermorite induced by humic acid and municipal solid waste incineration bottom ash upon hydrothermal treatment was reported and its potential application for efficient removal of Cu(II) ions was further investigated. Experimental results showed that the morphology and microstructure of IBA remarkably changed from sheet-like to particle-like after hydrothermal treatment, thereby resulting in substantial increases of sorption capacity and specific surface area. The synthesized tobermorite exhibited a strongly enhanced sorption performance toward Cu(II), which was 270.3 mg g<sup>-1</sup> and higher than other reported sorbents. The adsorption behaviors were examined by isotherm and kinetic studies. Langmuir model was found to describe the adsorption process well, suggesting that the adsorption was chemisorption in nature. Considering the very good results obtained for Cu(II), future studies can be addressed to evaluate the sorption capacity of the composite material with other heavy metals. In that case, the hydrothermally synthesized tobermorite may be used as sorbents to remove various heavy metals. Conversion of IBA into valuable minerals recovers waste into potential resources and alleviates the needs for ash disposal.

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**Table 1** Chemical compositions of incineration bottom ash (IBA) used in the current study.

Component	Content (wt.%)
CaO	54.06
$SiO_2$	8.24
$SO_3$	7.89
$Al_2O_3$	6.85
$P_2O_5$	4.83
Fe <sub>2</sub> O <sub>3</sub>	4.59
Cl	3.69
Na <sub>2</sub> O	2.55
MgO	2.38
$TiO_2$	1.75
$K_2O$	1.37
ZnO	0.79
CuO	0.25
BaO	0.24
MnO	0.16
PbO	0.10
$Cr_2O_3$	0.08
SrO	0.07
$SnO_2$	0.05
NiO	0.02
$ZrO_2$	0.02
Total	99.98

Table 2 Comparison of Cu(II) sorption capacity by IBAs and other sorbents.

Sorbents	Cu(II) sorbed (mg g <sup>-1</sup> )	Reference
Raw IBA	147.06	This study
Treated IBA	178.57	This study
IBA-HA complex	212.77	This study
Treated (IBA+HA)	270.27	This study
Activated carbon	37.17	Demiral et al., 2016
Granular sludge	25.70	Luo et al., 2014
Chitosan	64.62	Ngah et al., 2008
Biochar	10.26	Pellera et al., 2012
Zeolite	23.30	Wang et al., 2008
Bentonite	44.84	Veli et al., 2007
Goethite	10.70	Weng et al., 2008
Cellulose	63.09	Shen et al., 2009

# **Figure Captions**

**Fig. 1.** Morphology of (a) the raw IBA (top row); and (b) the corresponding hydrothermally treated IBA (bottom row).

**Fig. 2.** Morphology of (a) IBA mixed with HA before hydrothermal treatment (top row); (b) IBA mixed with 10 ppm HA after hydrothermal treatment (middle row); and (c) IBA mixed with 100 ppm HA after hydrothermal treatment (bottom row).

**Fig. 3.** UV-vis spectra of different species including HA sample, the raw and the hydrothermally treated IBA, and the IBA mixed with 100 ppm HA after hydrothermal treatment.

**Fig. 4.** FT-IR spectra of HA sample, the raw and the hydrothermally treated IBA, and the IBA mixed with 100 ppm HA after hydrothermal treatment.

**Fig. 5.** XRD diffractograms of the IBA samples mixed with and without different concentrations of HA before and after hydrothermal treatment. HA samples with 10 ppm and 100 ppm are used.

**Fig. 6.** N<sub>2</sub> adsorption-desorption isotherms of (a) IBA mixed with HA before and after hydrothermal treatment and (b) IBA with and without hydrothermal treatment at -196°C; (c) cumulative pore volume and (d) desorption BJH pore size distribution of IBA materials.

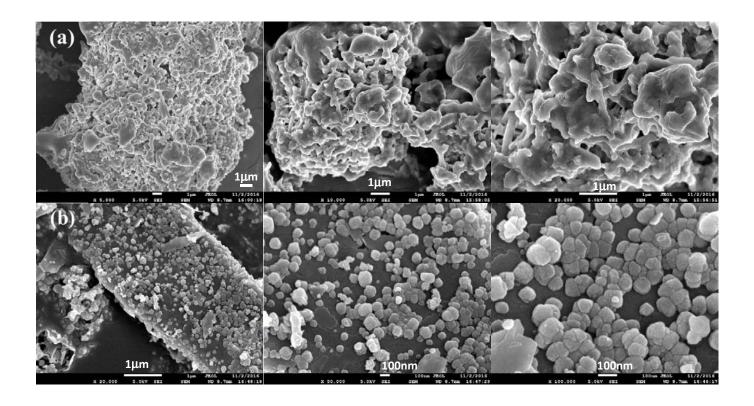


Fig. 1

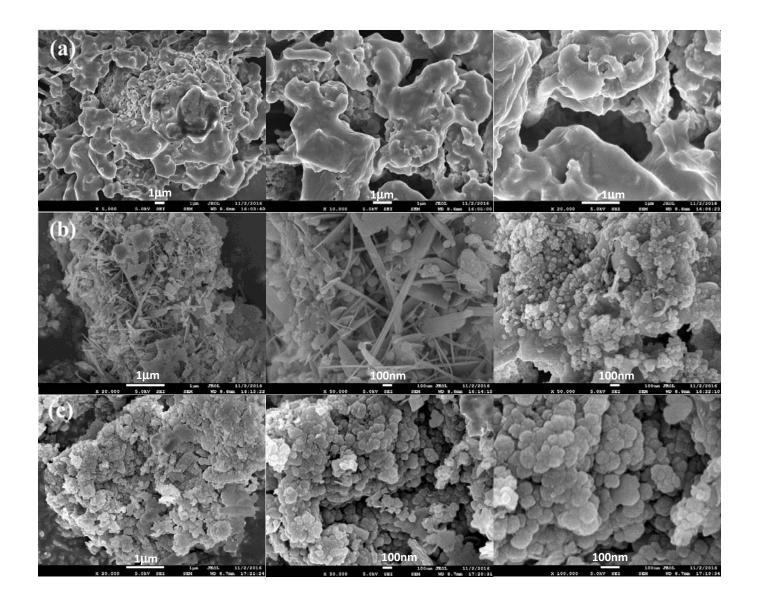


Fig. 2

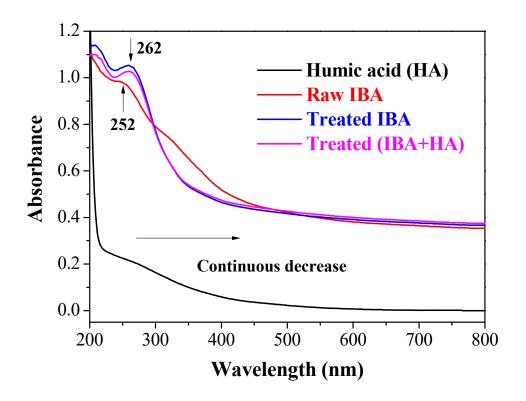


Fig. 3

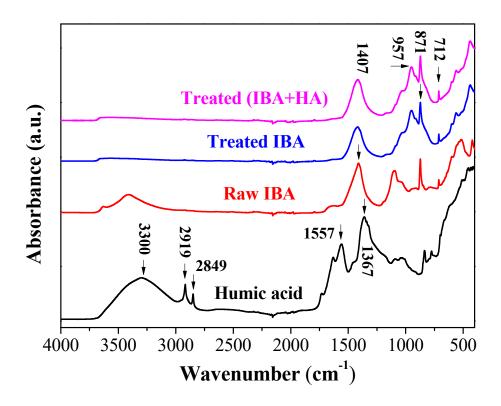


Fig. 4

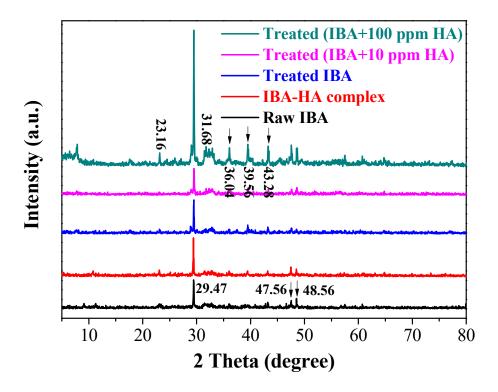


Fig. 5

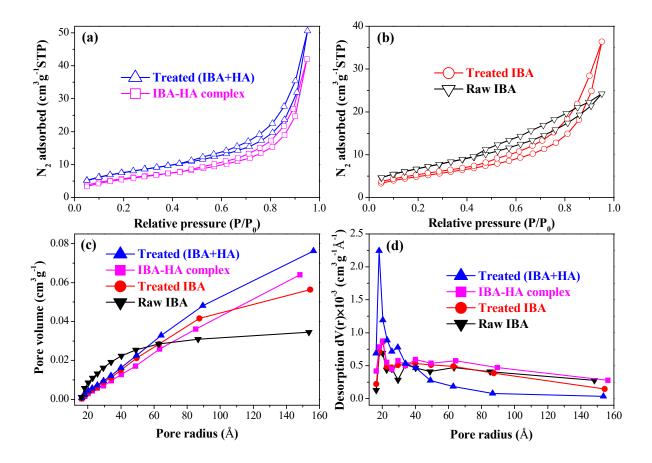


Fig. 6