

CO₂ Hydrogenation to Methanol on Tungsten-Doped Cu/CeO₂ Catalysts

Yong Yan, Roong Jien Wong, Zhirui Ma, Felix Donat, Shibo Xi, Syed Saqline, Qianwenhao Fan, Yonghua Du, Armando Borgna, Qian He, Christoph R. Müller, Wei Chen, Alexei A. Lapkin, Wen Liu¹

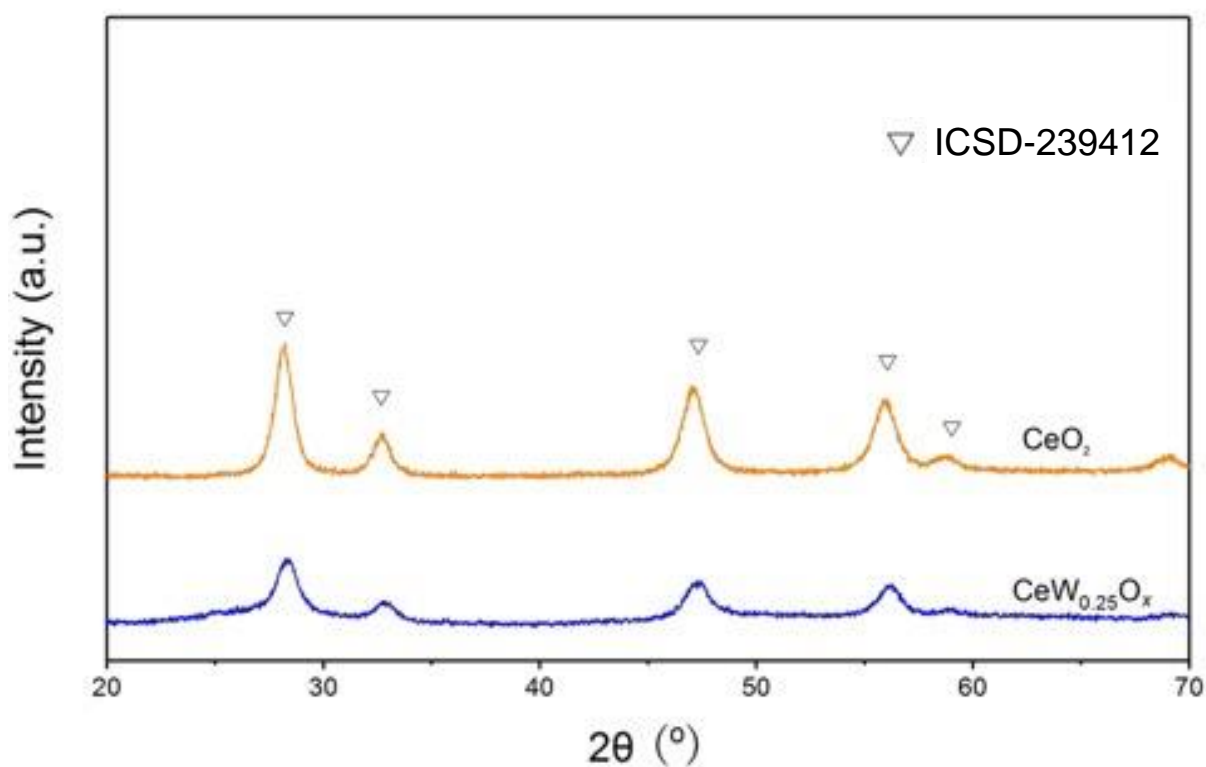


Figure S1. XRD patterns of as-calcined supports.

¹ Corresponding author: wenliu@ntu.edu.sg

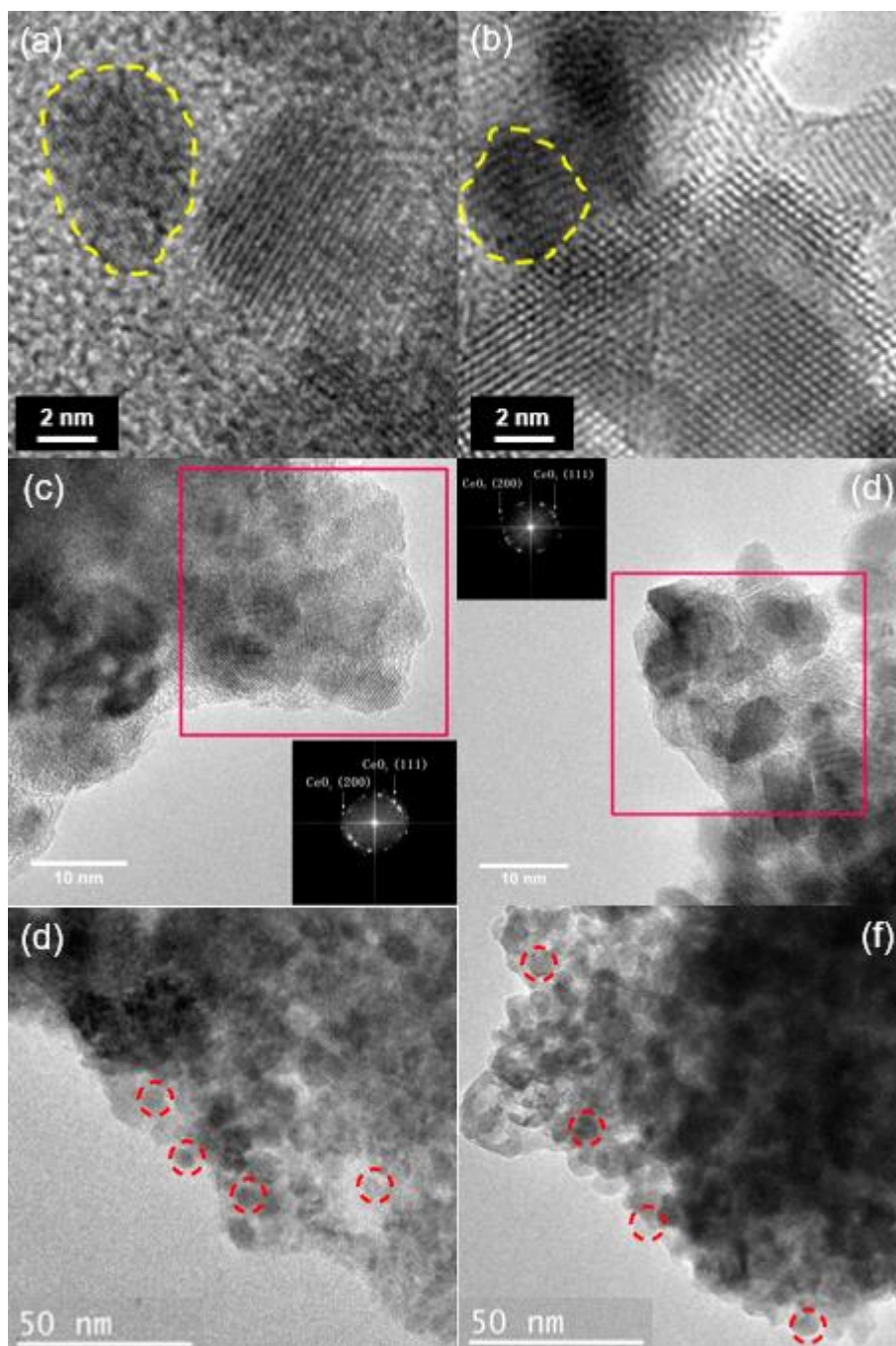


Figure S2. HRTEM images of (a, c, e) Cu/CeO₂ and (b, d, f) Cu/CeW_{0.25}O_x catalysts. The yellow outlines in (a) and (b) highlight grains of Cu. The insets in (c) and (d) show SAED of the selected areas in red. The red circles in (d) and (f) highlight Cu particles.

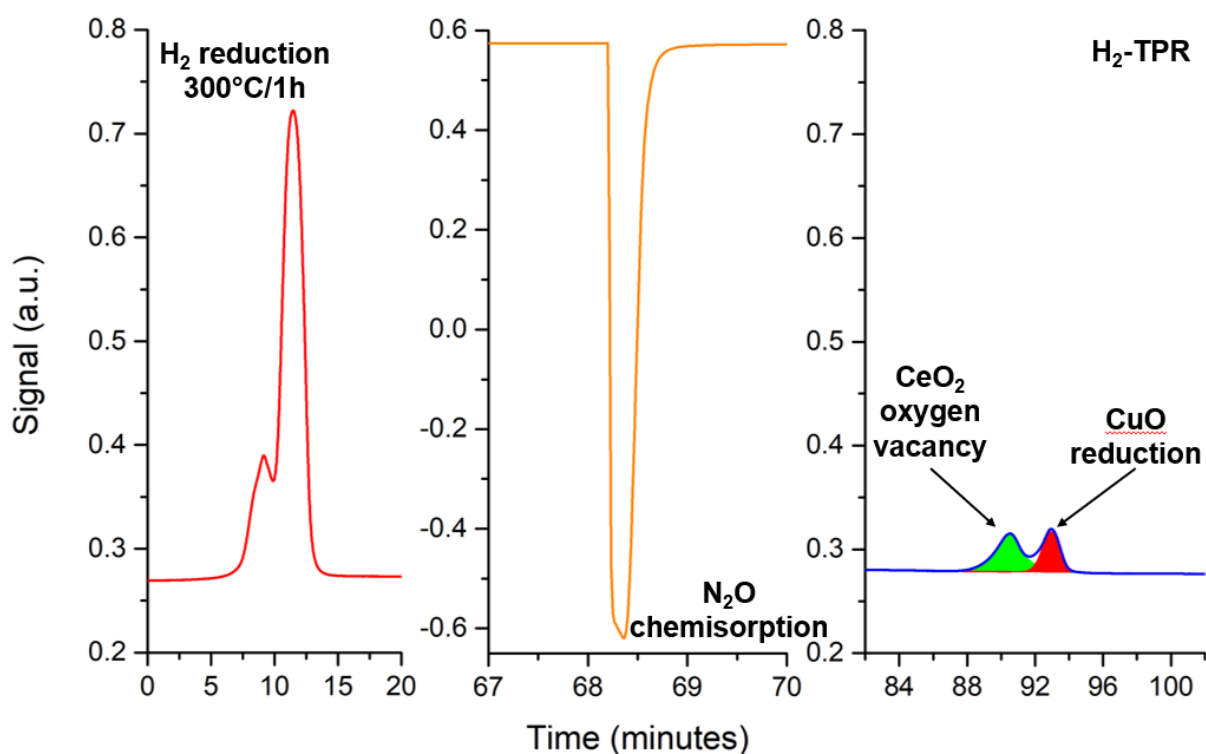


Figure S3. N_2O chemisorption profile of Cu/CeO_2 during (left) pre-reduction, (middle) N_2O chemisorption and (right) H_2 -TPR. The first peak during H_2 -TPR is assigned to the creation of oxygen vacancies on the CeO_2 support vacancy due to hydrogen spillover across the Cu/CeO_2 interface. Therefore, only the second TPR peak, which corresponds to the removal of surface oxygen monolayer from Cu particles, is used for estimating the Cu dispersion. CeO_2 oxygen vacancy peak was not observed in $\text{Cu}/\text{CeW}_{0.25}\text{O}_x$ during the H_2 -TPR stage.

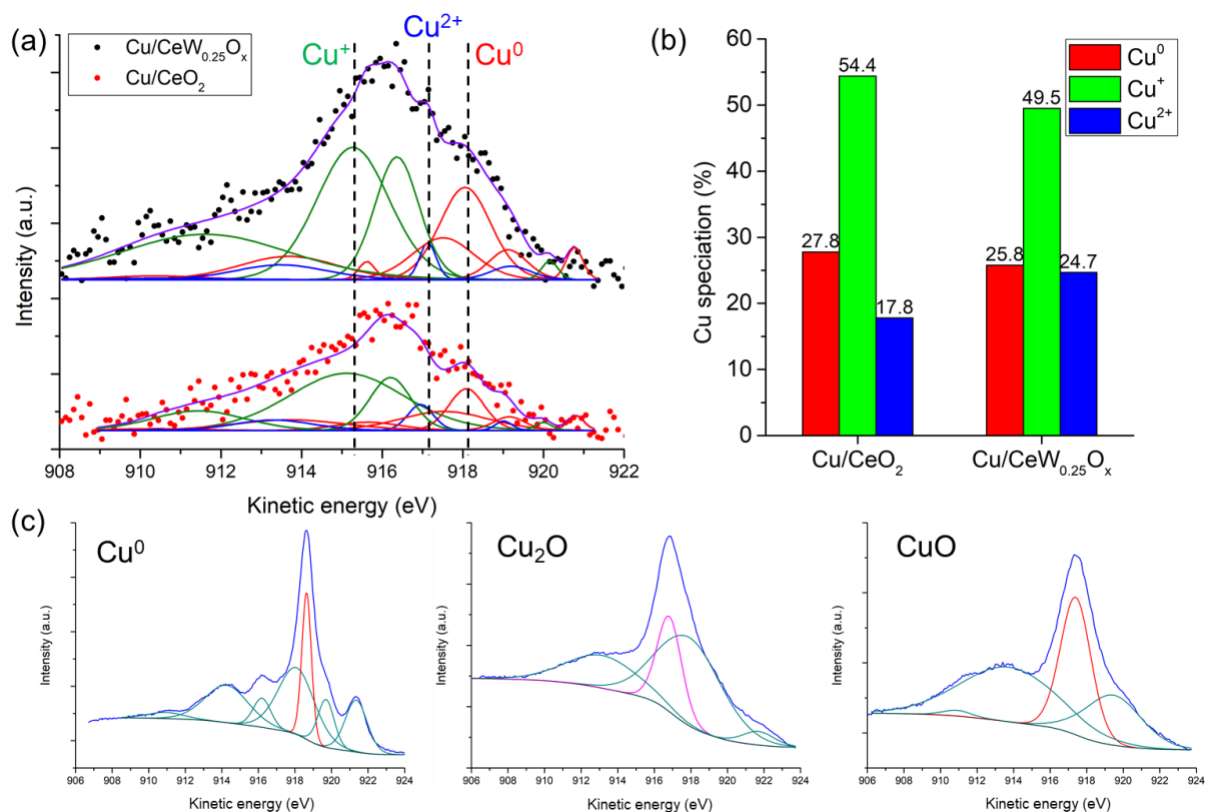


Figure S4. (a) Cu Auger spectra of Cu/CeO₂ and Cu/CeW_{0.25}O_x catalysts; the red, green, blue and purple curves represent the fitted profiles of Cu⁰, Cu⁺, Cu²⁺ and the sum of all fitted peaks, respectively. (b) Results of quantitative analysis of the Cu Auger spectra. (c) Reference Auger spectra of Cu⁰, Cu₂O, and CuO.

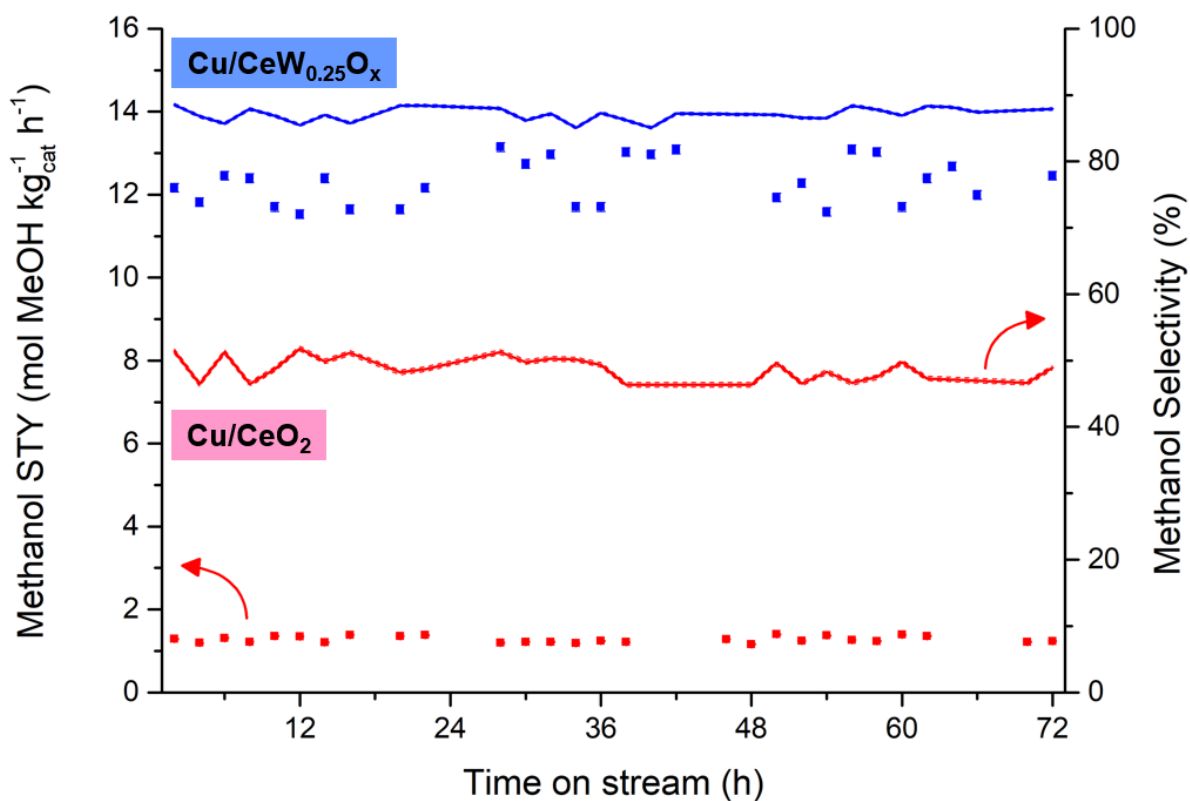


Figure S5. Methanol STY and selectivity over Cu/CeO₂ and Cu/CeW_{0.25}O_x catalysts during CO₂ hydrogenation in a 23:69:8 mixture of CO₂/H₂/N₂ at 250 °C, 35 bar, with a WHSV of 15000 mL g_{cat}⁻¹ h⁻¹, over 72 h time-on-stream. The dotted lines represent the 1 standard error of the methanol selectivities, estimated based on the variability between the data points.

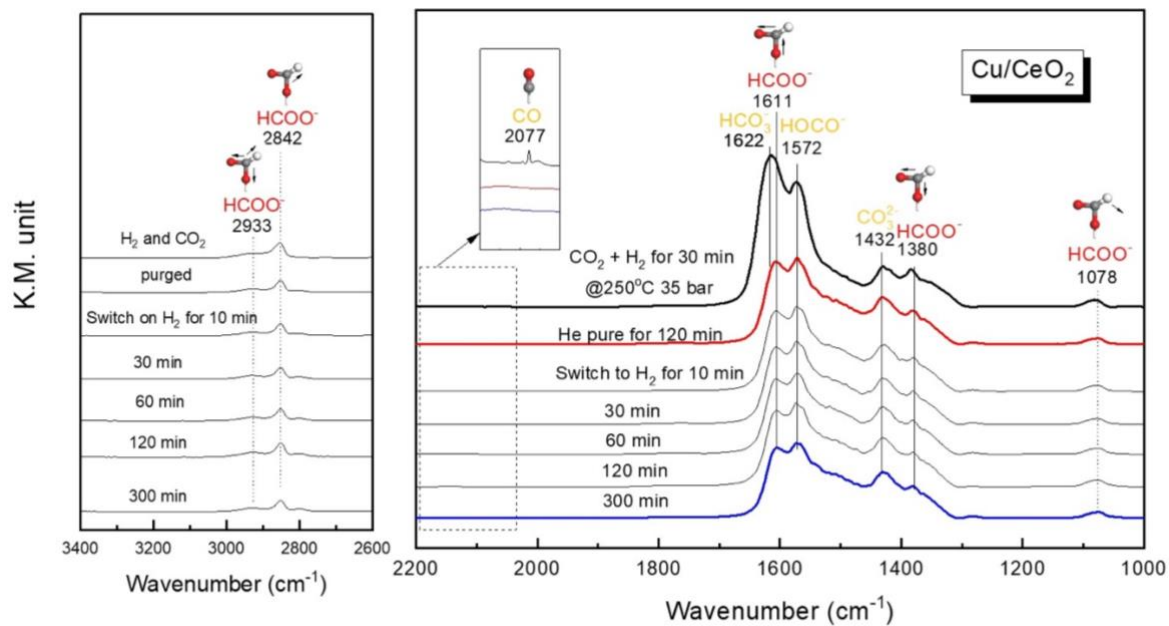


Figure S6. DRIFTS spectra recorded when Cu/CeO₂ was exposed to a 23:69:8 mixture of CO₂/H₂/N₂ at 250 °C for 30 min, followed by He purge for 120 min and then switching on H₂ only. All measurements were performed in 35 bar total pressure.

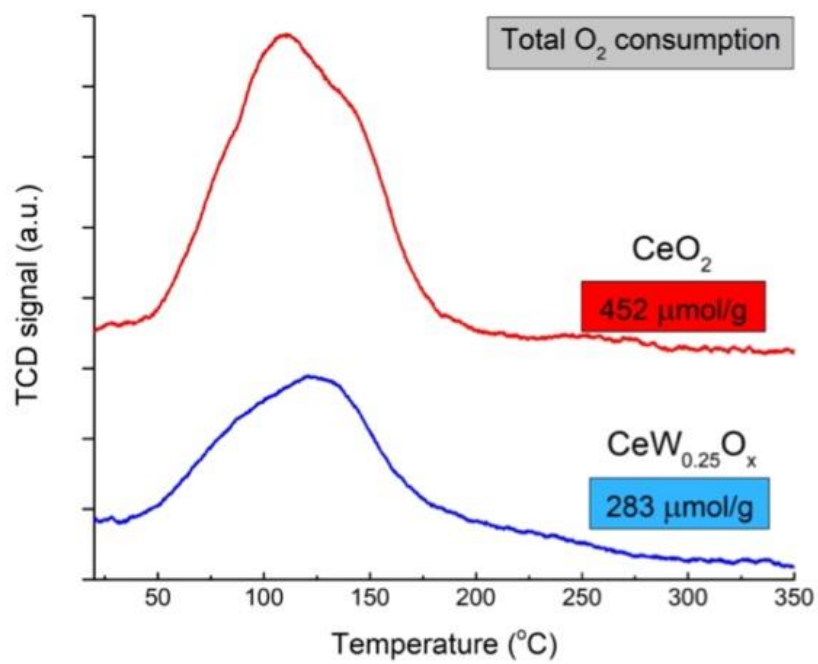


Figure S7. O_2 -TPO profiles of the pre-reduced supports.

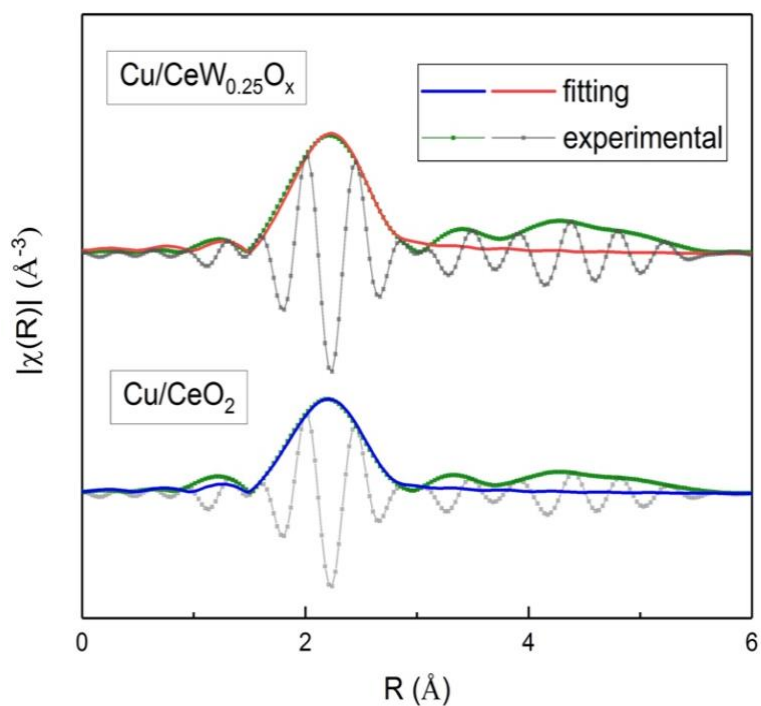


Figure S8. k_3 -weighted Fourier transforms of the Cu EXAFS data of the Cu/CeO_2 and $\text{Cu/CeW}_{0.25}\text{O}_x$ after reduction in 10% H_2/He at 500 °C, 10 bar total pressure.

Table S1. Results of ICP-OES analysis of Cu loading and N₂O chemisorption analysis of Cu dispersion on Cu/CeO₂ and Cu/CeW_{0.25}O_x.

Sample	Cu loading	Dispersion
Cu/CeO ₂	9.8 wt%	16.8 %
Cu/CeW _{0.25} O _x	10.9 wt%	16.9 %

Table S2. Comparison of the methanol synthesis activity of the Cu/CeO₂-based catalysts investigated in the present study and those reported in the literature.

Catalyst	Cu loading (wt.%)	T (°C)	P (MPa)	WHSV (mL g _{cat} ⁻¹ h ⁻¹)	H ₂ :CO ₂	Conv. (%)	Sel. (%)	STY		Ref
								mol _{MeOH} ·kg _{cat} ⁻¹ ·h ⁻¹	kg _{MeOH} ·kg _{cat} ⁻¹ ·h ⁻¹	
Cu/CeO ₂	9.8	250	3.5	15000	3	1.3	51	1.26	0.0403	This work
Cu/CeW _{0.25} O _x	10.9	250	3.5	15000	3	13	87	12.32	0.394	This work
Cu/CeTiO _x	25.5	235	3	2000	3	6.5	33	1.11	<u>0.0355</u>	[1]
Cu/CeO ₂	4.6	250	3	30000	3	1.6	50	2.1	0.0672	[2]
Cu/CeO ₂	8.9	300	5	45000	5	28	10	2.84	<u>0.0909</u>	[3]
Cu/CeO ₂	5	240	2	3000	3	2.1	90	0.636	<u>0.0204</u>	[4]
Cu/CeO ₂	35	280	3	10000	3	10.1	42	2.12	<u>0.0678</u>	[5]

Table S3. The apparent activation energy of both CO and methanol formation estimated from the Arrhenius-plot. The error estimated represents one standard deviation of the estimated Arrhenius constants.

Sample	$E_{a,\text{CO}}$ (kJ/mol)	$E_{a,\text{methanol}}$ (kJ/mol)
Cu/CeO ₂	54.8 ± 5.0	58.2 ± 2.1
Cu/CeW _{0.25} O _x	52.7 ± 2.5	38.0 ± 1.9

Table S4. The active oxygen vacancies obtained from CO₂-TPD profiles and the O₂ consumption by O₂-TPO.

Sample	CeO ₂	CeW _{0.25} O _x	Cu/CeO ₂	Cu/CeW _{0.25} O _x
Active vacancy volume (μmol/g)	144	103	121	78
O ₂ consumption (μmol/g)	452	283	-	-

Table S5. The mole fraction of Ce^{3+} in the catalysts at the various stages of in situ XANES experiment, estimated by the linear combination fitting analysis of the Ce L_{III} edge spectra.

Catalyst	Cu/CeO ₂	Ce/CeW _{0.25} O _x
Freshly calcined in air	0	49%
Reduced by H ₂	17%	69%
During CO ₂ hydrogenation	15%	59%

Table S6. The fitting parameters of Cu EXAFS.

Sample	Cu-Cu Coordination Number	R(Å)	δ^2	ΔE_0
Cu/CeO ₂	9.1	2.531	0.0129	4.059
Cu/CeW _{0.25} O _x	9.5	2.539	0.0058	5.429

References

- [1] K. Chang, T. Wang, J.G. Chen, Hydrogenation of CO₂ to methanol over CuCeTiO_x catalysts, *Applied Catalysis B: Environmental*. 206 (2017) 704–711. <https://doi.org/10.1016/j.apcatb.2017.01.076>.
- [2] J. Zhu, Y. Su, J. Chai, V. Muravev, N. Kosinov, E.J.M. Hensen, Mechanism and Nature of Active Sites for Methanol Synthesis from CO/CO₂ on Cu/CeO₂, *ACS Catal.* 10 (2020) 11532–11544. <https://doi.org/10.1021/acscatal.0c02909>.
- [3] P. Sripada, J. Kimpton, A. Barlow, T. Williams, S. Kandasamy, S. Bhattacharya, Investigating the dynamic structural changes on Cu/CeO₂ catalysts observed during CO₂ hydrogenation, *Journal of Catalysis*. 381 (2020) 415–426. <https://doi.org/10.1016/j.jcat.2019.11.017>.
- [4] B. Ouyang, W. Tan, B. Liu, Morphology effect of nanostructure ceria on the Cu/CeO₂ catalysts for synthesis of methanol from CO₂ hydrogenation, *Catalysis Communications*. 95 (2017) 36–39. <https://doi.org/10.1016/j.catcom.2017.03.005>.
- [5] W. Wang, Z. Qu, L. Song, Q. Fu, CO₂ hydrogenation to methanol over Cu/CeO₂ and Cu/ZrO₂ catalysts: Tuning methanol selectivity via metal-support interaction, *Journal of Energy Chemistry*. 40 (2020) 22–30. <https://doi.org/10.1016/j.jechem.2019.03.001>.